

Gas-Diffusion Electrodes for Carbon Dioxide Reduction: A New Paradigm

Drew Higgins,^{†,‡,⊥} Christopher Hahn,^{†,‡,⊥} Chengxiang Xiang,[§] Thomas F. Jaramillo,^{*,†,‡,⊥} and Adam Z. Weber^{*,⊥}

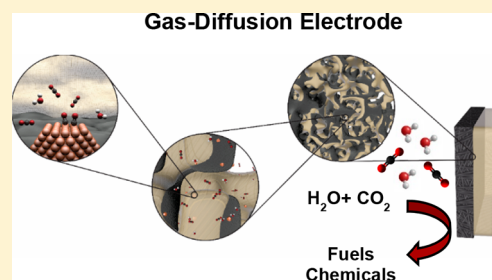
[†]Department of Chemical Engineering, Stanford University, 443 Via Ortega Way, Stanford, California 94305, United States

[‡]SUNCAT Center for Interface Science and Catalysis, SLAC National Accelerator Laboratory, 2575 Sand Hill Road, Menlo Park, California 94025, United States

[§]Division of Chemistry and Chemical Engineering, California Institute of Technology, 210 Noyes Laboratory, 127-72, Pasadena, California 91125, United States

[⊥]Energy Conversion Group, Energy Technologies Area, Lawrence Berkeley National Laboratory, 1 Cyclotron Road, MS70-108B, Berkeley, California 94720, United States

ABSTRACT: Significant advances have been made in recent years discovering new electrocatalysts and developing a fundamental understanding of electrochemical CO₂ reduction processes. This field has progressed to the point that efforts can now focus on translating this knowledge toward the development of practical CO₂ electrolyzers, which have the potential to replace conventional petrochemical processes as a sustainable route to produce fuels and chemicals. In this Perspective, we take a critical look at the progress in incorporating electrochemical CO₂ reduction catalysts into practical device architectures that operate using vapor-phase CO₂ reactants, thereby overcoming intrinsic limitations of aqueous-based systems. Performance comparison is made between state-of-the-art CO₂ electrolyzers and commercial H₂O electrolyzers—a well-established technology that provides realistic performance targets. Beyond just higher rates, vapor-fed reactors represent new paradigms for unprecedented control of local reaction conditions, and we provide a perspective on the challenges and opportunities for generating fundamental knowledge and achieving technological progress toward the development of practical CO₂ electrolyzers.



The development of new technologies that reduce greenhouse gas emissions while producing fuels and commodity chemicals has the potential to mitigate the devastating impacts of climate change by transforming the petrochemical sector toward sustainability. Electrochemical CO₂ reduction (CO₂R) coupled with renewably generated electricity (wind, solar, hydro) provides an attractive approach for the carbon-neutral production of valuable hydrocarbon, alcohol, and carbonyl products that find widespread use in the energy and chemical sectors. For this artificial photosynthesis process to be implemented at scale, highly active and selective CO₂R catalysts must be developed and ultimately integrated into devices that can achieve high conversion rates and energy-conversion efficiencies to the desired product(s). Vapor-fed CO₂ devices represent a promising platform for such a technology.

On a fundamental level, there has been much progress understanding electrochemical CO₂R in the liquid phase, where CO₂ molecules are solubilized in an aqueous electrolyte and reduced on the surface of a catalyst (Figure 1a). The unprecedented level of synergy between theoretical and experimental research toward aqueous-phase CO₂R has led

to improved understanding regarding the impact of electrolyte ions,^{1–3} pH,⁴ mass transport,^{5–7} temperature,⁸ and pressure^{8,9} on activity and selectivity. As a result, activity descriptors^{10,11} and mechanistic insight into reaction pathways^{12,13} have guided catalyst design efforts, leading to the discovery of new compositions^{14–16} and morphologies that are more active and selective to desired CO₂R products. A succinct overview of these advances has been provided in a recently published perspective piece.¹⁷ It is furthermore expected these efforts will be accelerated with the implementation of machine learning processes for catalyst discovery.^{18,19}

While the above referenced studies have been critical in establishing a deeper understanding of CO₂R, they have traditionally relied upon aqueous-phase CO₂R reactors designed for fundamental investigations (Figure 1a). From an applied standpoint, however, these test reactors have many practical limitations that must be addressed. Most notably, the poor solubility (ca. 34 mM) of CO₂ in aqueous electrolytes,

Received: October 24, 2018

Accepted: December 14, 2018

Published: December 14, 2018

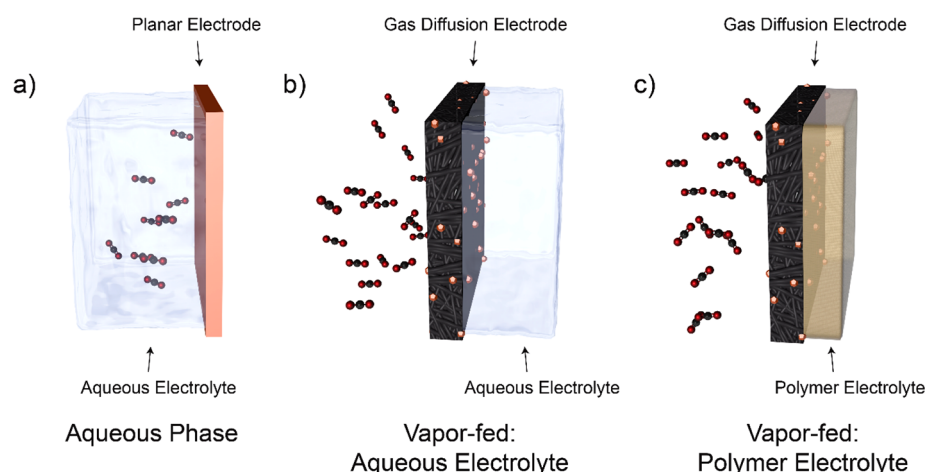


Figure 1. Different electrochemical CO₂R reactor schemes. (a) Aqueous-phase CO₂R, where CO₂ is first solubilized in an aqueous electrolyte and then reduced at a catalyst surface. Vapor-fed CO₂R employing an (b) aqueous or (c) polymer electrolyte.

Moving toward practical reactor designs that operate using CO₂ delivered to the cathode in the vapor phase can help to overcome these performance and solubility challenges.

along with acid/base buffer (CO₂/HCO₃⁻/CO₃²⁻) equilibria lead to intrinsic challenges toward achieving high conversion rates and energy efficiencies.²⁰ Moving toward practical reactor designs that operate using CO₂ delivered to the cathode in the vapor phase (Figure 1b,c) can help to overcome these performance and solubility challenges. Such gas-diffusion electrodes (GDEs) can achieve this by employing a porous catalyst layer along with diffusion media to facilitate reactant transport and distribution. GDEs have been used in other electrochemical energy-conversion devices such as fuel cells and electrolyzers, where the architecture has been optimized for high current density and low transport losses. However, the adaptation to CO₂R will require further advancement, as different operating strategies and understandings are needed to

address product selectivity considerations, which is important to avoid the need for costly downstream separations.²¹ Furthermore, the actual electrolyte can either be aqueous to form a catalyst/liquid electrolyte interface (Figure 1b), or ideally an ion-conducting polymer that can transport charged species (e.g., H⁺ or OH⁻) and form a catalyst/polymer-electrolyte interface (Figure 1c).

A recently published article²² provides a critical overview of various electrolyzer designs that can be considered, along with a review of the technological achievements made in recent years on electrochemical CO₂R reactor designs. In this Perspective, we discuss the challenges and opportunities facing GDE development for electrochemical CO₂R. We provide context in terms of CO₂R electrocatalysis, and include a discussion of the intrinsic advantages and unexpected opportunities of GDEs in an effort to motivate researchers to translate current understanding toward new GDE designs. The purpose of this Perspective is not to provide a comprehensive review on the topic of electrochemical CO₂R or GDE development. Instead, the goal is to provide a forward-looking perspective to inspire and provide direction for these fields of research, using the technology maturation process of

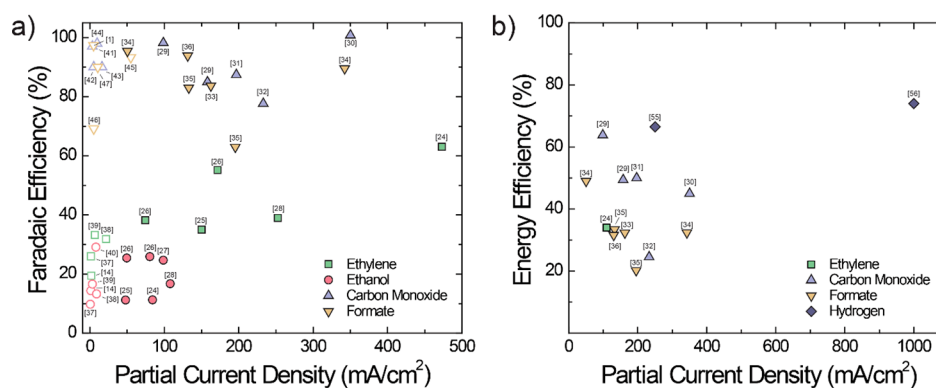


Figure 2. State-of-the-art performance of vapor-fed CO₂ devices. (a) Faradaic efficiencies versus partial current densities to ethylene, ethanol, carbon monoxide, and formate. (b) Energy efficiencies versus partial current densities to ethylene, carbon monoxide, formate, and hydrogen. Performances obtained for vapor-fed CO₂R electrodes are shown in solid symbols, while performance for electrodes in aqueous-phase CO₂R reactors are shown in hollow symbols. All energy efficiencies were calculated as voltage efficiencies using the formula: energy efficiency = $\frac{(E_{\text{anode}}^0 - E_{\text{cathode}}^0) \times \text{FE}}{V_{\text{cell}}}$, where E_{anode}^0 and E_{cathode}^0 are the reversible potentials, FE is the faradaic efficiency for the CO₂R product, and V_{cell} is the uncompensated cell voltage.

commercial water electrolyzers as realistic performance targets. We identify areas deemed important for developing a fundamental understanding of the underlying chemistry, processes, and phenomena occurring in GDEs. This insight is essential for advancing the state of electrochemical CO₂R technologies toward commercial viability.

State-of-the-Art. In comparison to electrodes studied in aqueous-phase electrochemical reactors, various types of vapor-fed CO₂R electrodes have been successful in improving the partial current densities and energy efficiencies for CO₂R.²³ This has been achieved by taking the most selective catalysts identified through fundamental aqueous-phase reactor investigations and integrating them into vapor-fed device designs. This research translation trend is depicted in Figure 2a, which summarizes state-of-the-art faradaic efficiencies versus partial current densities achieved for CO, formate, ethylene, and ethanol production. Performance obtained from vapor-fed GDEs^{24–36} (solid symbols) are shown in comparison to similar catalyst compositions tested in aqueous-phase reactors^{1,14,37–47} (hollow symbols). While different reactor designs and catalyst configurations were used throughout these studies, this comparison shows the general trend of vapor-fed GDE research successfully improving partial current densities beyond those achievable in aqueous-phase investigations, while retaining similar selectivity. Among these major products shown, the highest faradaic efficiencies and partial current densities are generally reported for CO and formate, as there are a number of different catalyst types that are intrinsically selective to these 2e[−] reduction products.^{36,48–52} On the other hand, data for the further reduced (>2e[−]) products, ethylene and ethanol, demonstrates that selectivity is still a major challenge. This selectivity challenge is largely because ethylene and ethanol are competitively coproduced on Cu-based catalysts through very similar mechanistic reaction pathways. However, improvements in ethylene selectivity have been observed by implementing Cu-based catalysts in vapor-fed GDEs for electrochemical CO₂R,^{24,26} along with similar results demonstrated for electrochemical carbon-monoxide reduction.^{53,54} This observation suggests that vapor-fed conditions are a promising avenue for tuning the local environment and reaction conditions that control CO₂R selectivity (*vide infra*), while simultaneously achieving higher partial current densities. However, altering the local CO₂ environment is largely underexplored for GDEs and presents an opportunity for

increased understanding compared to solely aqueous-phase reactor investigations.

On a system level, Figure 2b shows a summary of state-of-the-art energy efficiencies versus partial current densities, which takes into account transport resistances (ionic and electronic), along with kinetic losses from both the anode and cathode.⁵⁵ A comparison is also provided to the performance of representative alkaline⁵⁵ and proton-exchange membrane⁵⁶ (PEM) H₂O electrolyzers. It is interesting to note that all of the vapor-fed CO₂R cells incorporate an aqueous electrolyte (Figure 1b), in part because alkaline electrolytes can improve energy efficiencies by reducing cathodic overpotentials. Thus, a traditional commercial H₂O electrolyzer with an aqueous alkaline electrolyte⁵⁵ likely provides the most appropriate

The challenges and opportunities facing vapor-fed CO₂R electrode development relate to understanding and optimizing the multitude of processes occurring in three-dimensional GDEs. These processes span different length and time scales, with the complex interplay between phenomena ultimately having a governing effect on the CO₂ reaction selectivity and the energy-conversion efficiencies and rates.

comparison. While the representative alkaline H₂O electrolyzer performance is superior to that of the vapor-fed CO₂ cells shown in Figure 2b, the performance of CO₂R to CO cells has been recently closing the gap. Comparing CO₂R cell data to the representative PEM H₂O electrolyzer shows the intrinsic advantages of the PEM configuration (Figure 1c) for high current-density applications (Figure 2b) due to their more efficient reactant management, high reaction area, and minimal distances for ion transport. Clearly, there are opportunities to develop vapor-fed CO₂ devices in this configuration as there is currently a dearth of such studies. Moving forward, it is necessary to understand and optimize transport properties and reaction kinetics in vapor-fed CO₂R devices to advance the

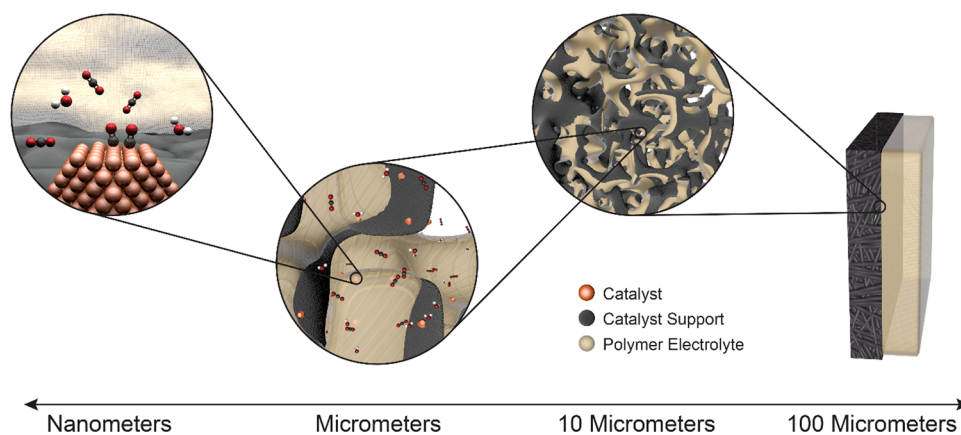


Figure 3. Schematic of a three-dimensional GDE depicting the multiple length scales where phenomena are occurring during electrochemical CO₂R.

performance toward practical viability. While we have focused on partial current density, Faradaic efficiency, and energy efficiency as immediately important performance figures of merit, we note that other parameters such as CO₂ utilization and component stability will also become increasingly important.

Challenges and Opportunities. A crucial first step in the development of vapor-fed CO₂R devices relates to engineering the GDE structures. Despite decades of studies, GDEs continue to be an active area of research in the fuel-cell sector, and performance improvements are still being realized through GDE optimization strategies that aim to address the many open questions that remain. GDEs in fuel cells may represent a simplified case in comparison to those in CO₂R cells, as reaction selectivity and different product phases (vapor versus liquid) are not as crucial considerations for fuel cells. The challenges and opportunities facing vapor-fed CO₂R electrode development relate to understanding and optimizing the multitude of processes occurring in three-dimensional GDEs. These processes span different length and time scales (Figure 3), with the complex interplay between phenomena ultimately having a governing effect on the CO₂ reaction selectivity and the energy-conversion efficiencies and rates. As these research efforts are accelerated, it will be necessary to translate fundamental knowledge from aqueous-phase CO₂R studies to vapor-fed systems and identify gaps and emergent phenomena. The vapor-fed systems are inherently more complex, due to the presence of a myriad of heterogeneous interfaces on the micro- and nanometer scales. Future research and scientific challenges must be addressed by closely coupled experimental and theoretical investigations. Areas deemed important for knowledge generation and technological process are outlined herein.

Transport of Reactants. In vapor-phase CO₂R electrodes, the delivery of relevant reaction species (CO₂, electrons, and H⁺) can be readily optimized to achieve improved conversion rates. Most notably, vapor-fed cells overcome the intrinsic solubility challenges of CO₂ in aqueous electrolytes (ca. 34 mM). At these low concentrations, mass-transport limitations significantly hinder CO₂ conversion rates in aqueous-phase devices when current densities exceed ca. 10 mA/cm².²⁰ The type of catalyst and GDE fabrication process must be carefully selected to maximize the catalytically active surface area available, and micro- and nanoscale electrode architectures must be designed to optimize CO₂, ion, and product transport simultaneously.⁵⁷ If present, the properties of the diffusion media, including porosity, pore structure, hydrophilicity, and thickness also play significant roles in governing electrode performance. These parameters have been explored and optimized in the case of fuel cells,⁵⁸ whereby H₂/O₂ fuel cells are able to reliably achieve current densities in excess of 1 A/cm². This provides a good basis for comparison, yet very limited understanding exists toward the design and development of high current density CO₂R electrodes, which must be established through concerted experimental and theoretical efforts.

The relative humidity and concentration of water in vapor-fed CO₂R reactors can be carefully controlled to overcome the intrinsic challenges associated with aqueous-phase CO₂R, where the concentration of water at the catalyst surface is ca. 55 M, whereas in a typical ion-exchange membrane, water concentrations on the order of 1–25 M or so are obtainable via humidity control although there is trade-off in ionic conductivity at low water contents.^{59–61} Water can be a

proton source for CO₂R as well as for the undesirable HER. As the reversible potentials for most electrochemical CO₂ reactions lie within 200 mV of the HER,³⁷ the HER provides competition to CO₂R by occupying electrocatalytically active sites and consuming electrons as well as the proton source, resulting in reduced CO₂ conversion rates and energy efficiencies toward the desired product(s). By delivering CO₂ to the cathode in the vapor-phase, the local partial pressure of CO₂ can be decoupled from the concentration of water (provided an ionic transport pathway remains), enabling strategies to steer selectivity by controlling reactant transport to tune the coverage of intermediates on the catalyst surface. The impact of CO₂ partial pressure on vapor-fed device performance is, however, not well understood and should be the focus of future studies. Parametric investigations on well-characterized GDEs should be conducted and closely coupled to the development of continuum mathematical models to understand transport processes throughout these 3-dimensional porous electrodes and identify their impact on performance.

Polymer Electrolyte and Ionomer: Charge Carrier Transport and Catalyst/Electrolyte Interfaces. As previously mentioned, a key challenge of aqueous-phase CO₂R is the CO₂/carbonate/bicarbonate buffering equilibria that limits the range of operational pH values for CO₂R, and convolutes an accurate depiction of the boundary-layer properties at the catalyst surface.²⁰ This leads to inflexibility in tuning the chemical properties of the catalyst/electrolyte interface, despite the importance of these chemical properties in dictating surface reaction kinetics, mechanisms, and charge-transport processes. For example, electrolyte pH is known to significantly impact CO₂R activity and selectivity. In particular, increased activity toward valuable C–C coupled products are favored at high pH values,^{4,62} which cannot be reliably achieved for aqueous-phase CO₂R due to the above-mentioned equilibria. This presents a valuable opportunity to develop and utilize polymer electrolytes that can operate in different pH regimes and may exhibit very different ion concentrations due to their thinness as well as background charge. Furthermore, advances in polymer electrolytes must be translated to the development of ionomers for incorporation throughout the three-dimensional structure of a GDE to create an interconnected thin-film network needed for ionic species transport. Despite similar structures, the behavior of ionomer thin films in an electrode can vary quite significantly from the bulk polymer,⁶⁰ and advances in their development and understanding are needed.

Solid-state polymer electrolytes (Figure 1c) pose many intrinsic advantages over liquid-phase electrolytes (Figure 1b). Particularly, simplified device designs requiring fewer auxiliary components for electrolyte circulation and replenishment, and the elimination of any mobile counterions other than protons and hydroxyls are ideal from a sustainability and CO₂ utilization standpoint. Vapor-fed GDE based devices employing polymer electrolytes also provide additional transport advantages versus aqueous electrolytes as they enable shorter distances between the anode and cathode,⁶³ thereby minimizing ohmic resistances through a “zero-gap” complete solid-state configuration. Avoiding the use of corrosive liquid electrolytes also poses several safety advantages, including avoiding the risk of leaking or heat-induced pressure buildup. Polymer electrolytes furthermore enable operation at higher pressures and potentially allow for differential pressures to be used between the two electrodes, as reactant crossover can be

suppressed.⁶³ Finally, they provide an opportunity for separation of volatile liquid-phase CO₂R products directly at the site of generation. For example, when targeting alcohol products, in comparison to aqueous-phase CO₂R, vapor-fed devices will avoid the formation of azeotropic alcohol/water mixtures that would require energy intensive downstream separation processes.²¹ Clearly there is an immense opportunity for the development of solid polymer electrolytes and their integration with vapor-fed CO₂R GDEs. Key challenges include designing and integrating new polymer electrolytes that simultaneously satisfy the requirements of low cost, high ionic conductivity and selectivity, resistance to reactant/product crossover, CO₂ tolerance, and long-term chemical and mechanical stability under operating conditions.

On the electrode level, the ionomer properties, including type (i.e., anionic, cationic), structure and catalyst/ionomer interactions strongly influence CO₂R activity and selectivity, where the tethering of the ionic groups hinder movement of their counterions as well as influence the reactivity of the ionic group themselves relative to their behavior in liquid electrolytes. Ionic species (e.g., H⁺, OH⁻, HCO₃⁻) transport in the ionomer phase is a crucial consideration, in addition to the distribution of the ionomer phase throughout the three-dimensional GDE structure. Particularly, optimized ionomer distributions can enable good charge species transport and active site utilization, while nonideal distributions can adversely affect performance through catalytic or transport resistances.⁶⁴ There also exist enticing opportunities to modify ionomer structures to accommodate functional or ionic species that can provide promotional CO₂R effects, such as increasing the local CO₂ concentration, decreasing selective site poisoning through blocky architectures,¹⁵ or impacting reaction mechanisms and routes through chemical modification⁶⁵ and field effects, where the local ion concentrations and distances can be more precisely controlled.²

While recent advances have enabled understanding of how different parameters (i.e., pH, electrolyte concentrations, catalyst functionalization) fundamentally affect aqueous-phase CO₂R catalysis, it is an opportune time to translate and validate this current state of understanding to highly porous vapor-fed GDEs. For example, polymer electrolytes exhibit different acid/base equilibria time constants than aqueous electrolytes due to the existence of the polymer backbone.⁶⁶ Furthermore, while one may obtain the desired high pH in aqueous electrolytes using high flow rates, this provides challenges from a practicality standpoint;²⁴ a similar effect may perhaps be obtained with polymer electrolytes since their thinness and possibility for high current-density operation result in large hydroxide fluxes and amounts in the electrode ionomer. Targeted approaches to understand polymer electrolyte effects, ionomer distributions, ionomer/catalyst interactions and charge-carrier transport properties must be carried out on model and/or prototype vapor-fed CO₂R systems, where the use of new polymer electrolytes and ionomers provide an increased ability to control and manipulate the local reaction environment at the catalyst surface. It is suggested that researchers leverage previous efforts on these topics reported in the fuel cell or electrolyzer literature, especially as anion-exchange membranes and ionomers become more prevalent and understood.

Opportunities for Fundamental Understanding. With the seemingly overwhelming number of factors that govern the multiscale processes and performance of a GDE, a detailed

understanding of these phenomena will require experimental approaches closely coupled with multiscale theoretical modeling and prediction. Comprehensive models do not currently exist that simultaneously capture and bridge quantum- and molecular-level dynamics with continuum models of reactant and product transport. The difficulty lies in the disparate length- and time-scales between these processes that require the combination of nonlinear partial differential equations with complex boundary conditions. Robust numerical techniques that can accomplish this are needed, which will enable the necessary multiprocess understanding and optimization that will be essential for guiding and understanding GDE approaches.

In terms of experimental approaches, the increasing complexity of vapor-fed devices necessitates the development and utilization of operando, in situ, and ex situ probes that probe interfacial phenomena in highly porous electrodes. For this, simplified vapor-fed cells can potentially be designed to deconvolute the influence of common experimental parameters.⁶⁷ This could serve to enable facile characterization and CO₂R evaluation of catalyst and electrode structures, which will accelerate the implementation of new GDE formulations in high-performance devices. Additionally, vapor-fed GDEs offer a promising platform for experimentally characterizing the multiscale properties of devices and processes occurring during operation. By minimizing the use of liquids, challenges associated with beam attenuation and refraction are avoided, enabling mechanistic probing of electrode processes using X-ray scattering, absorption, or photoelectron techniques. For example, the electronic or chemical structure of catalytically active surface sites in GDEs under reaction conditions can be probed by in situ X-ray absorption spectroscopy^{68–70} or in situ X-ray photoelectron spectroscopy,^{71,72} respectively; meanwhile the effects of electrode pore sizes, structures, and surface properties on microscale transport processes can be interrogated by X-ray computed tomography coupled with performance evaluation.^{73–77} Developing an improved understanding of the effects of operating conditions and GDE configurations on performance will provide opportunity to engineer devices to provide multivariable optimization for achieving unprecedented knowledge and performance.

Beyond GDE designs to optimize the multiscale processes underlying their operation, electrode integration into vapor-fed reactors provides an ideal opportunity for advanced understanding. The impact of operational parameters such as relative humidity, reactant flow rates, temperature, and device electrical potential on CO₂ conversion rates and efficiency remains largely unexplored, yet provide additional levers to tune performance and selectivity. The type of polymer electrolyte (proton exchange, anion exchange, bipolar) and anode design and materials are essential considerations for incorporating GDEs into working devices,^{78,79} and GDE compatibility with electrolytes and anodes must be understood. The stability of GDEs under operating conditions is also an important topic that has not been addressed in detail here or in the literature, because vapor-fed CO₂R electrode design is a relatively early stage field of research. Stable, long-term operation will be essential for achieving practicality of these devices. As these devices will ideally be coupled with renewable sources of power, the question of variability and how it relates to GDE performance and stability must also be understood and addressed. Furthermore, engineering vapor-fed GDEs to be capable of accommodating low-grade or dilute CO₂ feed

sources (e.g., atmospheric CO₂) improves the practicality of these devices to different applications and elucidation of these effects is important.

Particularly, there is an immense scientific opportunity to develop fundamental understanding of the multiscale processes occurring in three-dimensional GDEs, and to optimize GDE performance through rational engineering approaches.

Outlook. Recent efforts have demonstrated the potential of translating scientific advances made in electrochemical CO₂ reduction research toward the development of practical CO₂ electrolyzers. Key challenges and opportunities that remain involve the understanding and development of three-dimensional vapor-fed CO₂ reduction electrodes that can achieve high conversion rates and energy efficiencies toward the desired products. Particularly, there is an immense scientific opportunity to develop fundamental understanding of the multiscale processes occurring in three-dimensional GDEs, and to optimize GDE performance through rational engineering approaches. Closely integrated experimental and theoretic investigations are required to progress upon our current state of understanding and perpetuate the advancement of CO₂ electrolyzers toward practical relevance. The knowledge generated and progress made in catalyst integration, electrode engineering, and electrochemical device design will also be directly applicable to other electrochemical conversion devices that could be of technological importance in the near future to replace gigatonne-scale, carbon-intensive industrial processes. These include sustainable electrochemical technologies for the production of fuels and chemicals from carbon-based feedstocks, or the synthesis of ammonia-based fertilizers from ambient N₂.

AUTHOR INFORMATION

Corresponding Authors

*E-mail: jaramillo@stanford.edu.

*E-mail: azweber@lbl.gov.

ORCID

Drew Higgins: 0000-0002-0585-2670

Christopher Hahn: 0000-0002-2772-6341

Chengxiang Xiang: 0000-0002-1698-6754

Thomas F. Jaramillo: 0000-0001-9900-0622

Adam Z. Weber: 0000-0002-7749-1624

Author Contributions

[†]D.H. and C.H.: Equal author contributions.

Notes

The authors declare no competing financial interest.

Biographies

Drew Higgins has been at Stanford University and SLAC National Laboratory since 2015, first as a Banting Postdoctoral Fellow and then Associate Staff Scientist working on electrochemical catalyst development, understanding and device integration. In January 2019, he starts a Faculty position at McMaster University in the Department of Chemical Engineering. <https://www.higginslab.com/>.

Christopher Hahn began his current position at SLAC National Accelerator Laboratory in 2015, where he is conducting research with the Joint Center for Artificial Photosynthesis on catalyst discovery and understanding reaction mechanisms for electrochemical CO₂ reduction. <https://suncat.stanford.edu/people/christopher-hahn>.

Chengxiang (“CX”) Xiang and his team are working on development of testbed prototypes for photoelectrochemical CO₂ reduction and water-splitting. <http://sunlight.caltech.edu/cx/>.

Thomas Jaramillo is an Associate Professor at Stanford and SLAC National Accelerator Laboratory and is a Thrust Coordinator in JCAP overseeing electrocatalysis research. His laboratory focuses on fundamental catalytic processes occurring on solid-state surfaces in both the production and consumption of energy. <http://jaramillogroup.stanford.edu/>.

Adam Weber is currently a Staff Scientist at LBNL where he leads the Energy Conversion Group and is a Thrust Coordinator in JCAP overseeing continuum modeling, multicomponent integration, and test-bed construction and evaluation. He is a Fellow of the Electrochemical Society for his research on understanding electrochemical technologies. <https://weberlab.lbl.gov/>.

ACKNOWLEDGMENTS

This work was supported by the Joint Center for Artificial Photosynthesis, a DOE Energy Innovation Hub, supported through the Office of Science of the U.S. Department of Energy under Award Number DE-SC0004993.

REFERENCES

- (1) Hori, Y. Electrochemical CO₂ Reduction on Metal Electrodes. In *Modern Aspects of Electrochemistry*; Vayenas, C. G., White, R. E., Gamboa-Aldeco, M. E., Eds.; Springer: New York, 2008; pp 89–189.
- (2) Resasco, J.; Chen, L. D.; Clark, E.; Tsai, C.; Hahn, C.; Jaramillo, T. F.; Chan, K.; Bell, A. T. Promoter Effects of Alkali Metal Cations on the Electrochemical Reduction of Carbon Dioxide. *J. Am. Chem. Soc.* **2017**, *139* (32), 11277–11287.
- (3) Resasco, J.; Lum, Y.; Clark, E.; Zeledon, J. Z.; Bell, A. T. Effects of Anion Identity and Concentration on Electrochemical Reduction of CO₂. *ChemElectroChem* **2018**, *5* (7), 1064–1072.
- (4) Wang, L.; Nitopi, S. A.; Bertheussen, E.; Orazov, M.; Morales-Guio, C. G.; Liu, X.; Higgins, D. C.; Chan, K.; Nørskov, J. K.; Hahn, C.; et al. Electrochemical Carbon Monoxide Reduction on Polycrystalline Copper: Effects of Potential, Pressure, and PH on Selectivity toward Multicarbon and Oxygenated Products. *ACS Catal.* **2018**, *8*, 7445–7454.
- (5) Singh, M. R.; Goodpaster, J. D.; Weber, A. Z.; Head-Gordon, M.; Bell, A. T. Mechanistic Insights into Electrochemical Reduction of CO₂ over Ag Using Density Functional Theory and Transport Models. *Proc. Natl. Acad. Sci. U. S. A.* **2017**, *114* (42), E8812.
- (6) Lobaccaro, P.; Singh, M. R.; Clark, E. L.; Kwon, Y.; Bell, A. T.; Ager, J. W. Effects of Temperature and Gas-Liquid Mass Transfer on the Operation of Small Electrochemical Cells for the Quantitative Evaluation of CO₂ Reduction Electrocatalysts. *Phys. Chem. Chem. Phys.* **2016**, *18* (38), 26777–26785.
- (7) Hashiba, H.; Weng, L.-C.; Chen, Y.; Sato, H. K.; Yotsuhashi, S.; Xiang, C.; Weber, A. Z. Effects of Electrolyte Buffer Capacity on Surface Reactant Species and the Reaction Rate of CO₂ in Electrochemical CO₂ Reduction. *J. Phys. Chem. C* **2018**, *122* (7), 3719–3726.
- (8) Hashiba, H.; Yotsuhashi, S.; Deguchi, M.; Yamada, Y. Systematic Analysis of Electrochemical CO₂ Reduction with Various Reaction Parameters Using Combinatorial Reactors. *ACS Comb. Sci.* **2016**, *18* (4), 203–208.
- (9) Ahn, S. T.; Abu-Baker, I.; Palmore, G. T. R. Electroreduction of CO₂ on Polycrystalline Copper: Effect of Temperature on Product Selectivity. *Catal. Today* **2017**, *288*, 24–29.

- (10) Liu, X.; Xiao, J.; Peng, H.; Hong, X.; Chan, K.; Nørskov, J. K. Understanding Trends in Electrochemical Carbon Dioxide Reduction Rates. *Nat. Commun.* **2017**, *8*, 15438.
- (11) Rendón-Calle, A.; Builes, S.; Calle-Vallejo, F. A Brief Review of the Computational Modeling of CO₂ Electroreduction on Cu Electrodes. *Curr. Opin. Electrochem.* **2018**, *9*, 158.
- (12) Garza, A. J.; Bell, A. T.; Head-Gordon, M. Mechanism of CO₂ Reduction at Copper Surfaces: Pathways to C₂ Products. *ACS Catal.* **2018**, *8* (2), 1490–1499.
- (13) Kortlever, R.; Shen, J.; Schouten, K. J. P.; Calle-Vallejo, F.; Koper, M. T. M. Catalysts and Reaction Pathways for the Electrochemical Reduction of Carbon Dioxide. *J. Phys. Chem. Lett.* **2015**, *6* (20), 4073–4082.
- (14) Clark, E. L.; Hahn, C.; Jaramillo, T. F.; Bell, A. T. Electrochemical CO₂ Reduction over Compressively Strained CuAg Surface Alloys with Enhanced Multi-Carbon Oxygenate Selectivity. *J. Am. Chem. Soc.* **2017**, *139* (44), 15848–15857.
- (15) Han, Z.; Kortlever, R.; Chen, H.-Y.; Peters, J. C.; Agapie, T. CO₂ Reduction Selective for C ≥ 2 Products on Polycrystalline Copper with N-Substituted Pyridinium Additives. *ACS Cent. Sci.* **2017**, *3* (8), 853–859.
- (16) Higgins, D.; Landers, A. T.; Ji, Y.; Nitopi, S.; Morales-Guio, C. G.; Wang, L.; Chan, K.; Hahn, C.; Jaramillo, T. F. Guiding Electrochemical Carbon Dioxide Reduction toward Carbonyls Using Copper Silver Thin Films with Interphase Miscibility. *ACS Energy Lett.* **2018**, *3*, 2947–2955.
- (17) Raciti, D.; Wang, C. Recent Advances in CO₂ Reduction Electrocatalysis on Copper. *ACS Energy Lett.* **2018**, *3* (7), 1545–1556.
- (18) De Luna, P.; Wei, J.; Bengio, Y.; Aspuru-Guzik, A.; Sargent, E. Use Machine Learning to Find Energy Materials. *Nature* **2017**, *552* (7683), 23.
- (19) Ulissi, Z. W.; Tang, M. T.; Xiao, J.; Liu, X.; Torelli, D. A.; Karamad, M.; Cummins, K.; Hahn, C.; Lewis, N. S.; Jaramillo, T. F.; et al. Machine-Learning Methods Enable Exhaustive Searches for Active Bimetallic Facets and Reveal Active Site Motifs for CO₂ Reduction. *ACS Catal.* **2017**, *7* (10), 6600–6608.
- (20) Singh, M. R.; Clark, E. L.; Bell, A. T. Effects of Electrolyte, Catalyst, and Membrane Composition and Operating Conditions on the Performance of Solar-Driven Electrochemical Reduction of Carbon Dioxide. *Phys. Chem. Chem. Phys.* **2015**, *17* (29), 18924–18936.
- (21) Greenblatt, J. B.; Miller, D. J.; Ager, J. W.; Houle, F. A.; Sharp, I. D. The Technical and Energetic Challenges of Separating (Photo)Electrochemical Carbon Dioxide Reduction Products. *Joule* **2018**, *2* (3), 381–420.
- (22) Weekes, D. M.; Salvatore, D. A.; Reyes, A.; Huang, A.; Berlinguette, C. P. Electrolytic CO₂ Reduction in a Flow Cell. *Acc. Chem. Res.* **2018**, *51* (4), 910–918.
- (23) Jhong, H.-R. M.; Ma, S.; Kenis, P. J. A. Electrochemical Conversion of CO₂ to Useful Chemicals: Current Status, Remaining Challenges, and Future Opportunities. *Curr. Opin. Chem. Eng.* **2013**, *2* (2), 191–199.
- (24) Dinh, C.-T.; Burdyny, T.; Kibria, M. G.; Seifitokaldani, A.; Gabardo, C. M.; García de Arquer, F. P.; Kiani, A.; Edwards, J. P.; De Luna, P.; Bushuyev, O. S.; et al. CO₂ Electroreduction to Ethylene Via Hydroxide-Mediated Copper Catalysis at an Abrupt Interface. *Science* **2018**, *360* (6390), 783–787.
- (25) Ma, S.; Sadakiyo, M.; Luo, R.; Heima, M.; Yamauchi, M.; Kenis, P. J. A. One-Step Electrosynthesis of Ethylene and Ethanol from CO₂ in an Alkaline Electrolyzer. *J. Power Sources* **2016**, *301*, 219–228.
- (26) Hoang, T. T. H.; Verma, S.; Ma, S.; Fister, T. T.; Timoshenko, J.; Frenkel, A. I.; Kenis, P. J. A.; Gewirth, A. A. Nanoporous Copper–Silver Alloys by Additive-Controlled Electrodeposition for the Selective Electroreduction of CO₂ to Ethylene and Ethanol. *J. Am. Chem. Soc.* **2018**, *140* (17), 5791–5797.
- (27) Zhuang, T.-T.; Liang, Z.-Q.; Seifitokaldani, A.; Li, Y.; De Luna, P.; Burdyny, T.; Che, F.; Meng, F.; Min, Y.; Quintero-Bermudez, R.; et al. Steering Post-C–C Coupling Selectivity Enables High Efficiency Electroreduction of Carbon Dioxide to Multi-Carbon Alcohols. *Nature Catalysis* **2018**, *1* (6), 421–428.
- (28) Lv, J.-J.; Jouny, M.; Luc, W.; Zhu, W.; Zhu, J.-J.; Jiao, F. A Highly Porous Copper Electrocatalyst for Carbon Dioxide Reduction. *Adv. Mater.* **2018**, *30* (49), 1803111.
- (29) Verma, S.; Hamasaki, Y.; Kim, C.; Huang, W.; Lu, S.; Jhong, H.-R. M.; Gewirth, A. A.; Fujigaya, T.; Nakashima, N.; Kenis, P. J. A. Insights into the Low Overpotential Electroreduction of CO₂ to CO on a Supported Gold Catalyst in an Alkaline Flow Electrolyzer. *ACS Energy Lett.* **2018**, *3* (1), 193–198.
- (30) Ma, S.; Luo, R.; Gold, J. I.; Yu, A. Z.; Kim, B.; Kenis, P. J. A. Carbon Nanotube Containing Ag Catalyst Layers for Efficient and Selective Reduction of Carbon Dioxide. *J. Mater. Chem. A* **2016**, *4* (22), 8573–8578.
- (31) Dufek, E. J.; Lister, T. E.; Stone, S. G.; McIlwain, M. E. Operation of a Pressurized System for Continuous Reduction of CO₂. *J. Electrochem. Soc.* **2012**, *159* (9), F514–F517.
- (32) Haas, T.; Krause, R.; Weber, R.; Demler, M.; Schmid, G. Technical Photosynthesis Involving CO₂ Electrolysis and Fermentation. *Nature Catalysis* **2018**, *1* (1), 32–39.
- (33) Whipple, D. T.; Finke, E. C.; Kenis, P. J. A. Microfluidic Reactor for the Electrochemical Reduction of Carbon Dioxide: The Effect of Ph. *Electrochem. Solid-State Lett.* **2010**, *13* (9), B109–B111.
- (34) Lu, X.; Leung, D. Y. C.; Wang, H.; Xuan, J. A High Performance Dual Electrolyte Microfluidic Reactor for the Utilization of CO₂. *Appl. Energy* **2017**, *194*, 549–559.
- (35) Li, H.; Oloman, C. Development of a Continuous Reactor for the Electro-Reduction of Carbon Dioxide to Formate – Part 2: Scale-Up. *J. Appl. Electrochem.* **2007**, *37* (10), 1107–1117.
- (36) Yang, H.; Kaczur, J. J.; Sajjad, S. D.; Masel, R. I. Electrochemical Conversion of CO₂ to Formic Acid Utilizing Sustainion Membranes. *J. CO₂ Utilization* **2017**, *20*, 208–217.
- (37) Kuhl, K. P.; Cave, E. R.; Abram, D. N.; Jaramillo, T. F. New Insights into the Electrochemical Reduction of Carbon Dioxide on Metallic Copper Surfaces. *Energy Environ. Sci.* **2012**, *5* (5), 7050–7059.
- (38) Jiang, K.; Sandberg, R. B.; Akey, A. J.; Liu, X.; Bell, D. C.; Nørskov, J. K.; Chan, K.; Wang, H. Metal Ion Cycling of Cu Foil for Selective C–C Coupling in Electrochemical CO₂ Reduction. *Nature Catalysis* **2018**, *1* (2), 111–119.
- (39) Kim, D.; Kley, C. S.; Li, Y.; Yang, P. Copper Nanoparticle Ensembles for Selective Electroreduction of CO₂ to C₂–C₃ Products. *Proc. Natl. Acad. Sci. U. S. A.* **2017**, *114* (40), 10560–10565.
- (40) Ren, D.; Ang, B. S.-H.; Yeo, B. S. Tuning the Selectivity of Carbon Dioxide Electroreduction toward Ethanol on Oxide-Derived Cu₂O Catalysts. *ACS Catal.* **2016**, *6* (12), 8239–8247.
- (41) Cave, E. R.; Montoya, J. H.; Kuhl, K. P.; Abram, D. N.; Hatsukade, T.; Shi, C.; Hahn, C.; Nørskov, J. K.; Jaramillo, T. F. Electrochemical CO₂ Reduction on Au Surfaces: Mechanistic Aspects Regarding the Formation of Major and Minor Products. *Phys. Chem. Chem. Phys.* **2017**, *19* (24), 15856–15863.
- (42) Hatsukade, T.; Kuhl, K. P.; Cave, E. R.; Abram, D. N.; Jaramillo, T. F. Insights into the Electrocatalytic Reduction of CO₂ on Metallic Silver Surfaces. *Phys. Chem. Chem. Phys.* **2014**, *16* (27), 13814–13819.
- (43) Lu, Q.; Rosen, J.; Zhou, Y.; Hutchings, G. S.; Kimmel, Y. C.; Chen, J. G.; Jiao, F. A Selective and Efficient Electrocatalyst for Carbon Dioxide Reduction. *Nat. Commun.* **2014**, *5*, 3242.
- (44) Chen, Y.; Li, C. W.; Kanan, M. W. Aqueous CO₂ Reduction at Very Low Overpotential on Oxide-Derived Au Nanoparticles. *J. Am. Chem. Soc.* **2012**, *134* (49), 19969–19972.
- (45) Zheng, X.; De Luna, P.; García de Arquer, F. P.; Zhang, B.; Becknell, N.; Ross, M. B.; Li, Y.; Banis, M. N.; Li, Y.; Liu, M.; et al. Sulfur-Modulated Tin Sites Enable Highly Selective Electrochemical Reduction of CO₂ to Formate. *Joule* **2017**, *1* (4), 794–805.
- (46) Feaster, J. T.; Shi, C.; Cave, E. R.; Hatsukade, T.; Abram, D. N.; Kuhl, K. P.; Hahn, C.; Nørskov, J. K.; Jaramillo, T. F. Understanding Selectivity for the Electrochemical Reduction of Carbon Dioxide to

Formic Acid and Carbon Monoxide on Metal Electrodes. *ACS Catal.* **2017**, *7* (7), 4822–4827.

(47) Gao, S.; Lin, Y.; Jiao, X.; Sun, Y.; Luo, Q.; Zhang, W.; Li, D.; Yang, J.; Xie, Y. Partially Oxidized Atomic Cobalt Layers for Carbon Dioxide Electroreduction to Liquid Fuel. *Nature* **2016**, *529*, 68.

(48) Zhao, S.; Jin, R.; Jin, R. Opportunities and Challenges in CO₂ Reduction by Gold- and Silver-Based Electrocatalysts: From Bulk Metals to Nanoparticles and Atomically Precise Nanoclusters. *ACS Energy Lett.* **2018**, *3* (2), 452–462.

(49) Cai, Z.; Wu, Y.; Wu, Z.; Yin, L.; Weng, Z.; Zhong, Y.; Xu, W.; Sun, X.; Wang, H. Unlocking Bifunctional Electrocatalytic Activity for CO₂ Reduction Reaction by Win-Win Metal–Oxide Cooperation. *ACS Energy Lett.* **2018**, *3* (11), 2816–2822.

(50) Lu, X.; Wu, Y.; Yuan, X.; Huang, L.; Wu, Z.; Xuan, J.; Wang, Y.; Wang, H. High-Performance Electrochemical CO₂ Reduction Cells Based on Non-Noble Metal Catalysts. *ACS Energy Lett.* **2018**, *3* (10), 2527–2532.

(51) Kaczur, J. J.; Yang, H.; Liu, Z.; Sajjad, S. D.; Masel, R. I. Carbon Dioxide and Water Electrolysis Using New Alkaline Stable Anion Membranes. *Front. Chem.* **2018**, *6*, 263.

(52) Salvatore, D. A.; Weekes, D. M.; He, J.; Dettelbach, K. E.; Li, Y. C.; Mallouk, T. E.; Berlinguette, C. P. Electrolysis of Gaseous CO₂ to CO in a Flow Cell with a Bipolar Membrane. *ACS Energy Lett.* **2018**, *3* (1), 149–154.

(53) Ripatti, D. S.; Veltman, T. R.; Kanan, M. W. Carbon Monoxide Gas Diffusion Electrolysis That Produces Concentrated C₂ Products with High Single-Pass Conversion. *Joule* **2018**, DOI: 10.1016/j.joule.2018.10.007.

(54) Jouny, M.; Luc, W.; Jiao, F. High-Rate Electroreduction of Carbon Monoxide to Multi-Carbon Products. *Nature Catal.* **2018**, *1* (10), 748–755.

(55) Zeng, K.; Zhang, D. Recent Progress in Alkaline Water Electrolysis for Hydrogen Production and Applications. *Prog. Energy Combust. Sci.* **2010**, *36* (3), 307–326.

(56) Carmo, M.; Fritz, D. L.; Mergel, J.; Stolten, D. A Comprehensive Review on Pem Water Electrolysis. *Int. J. Hydrogen Energy* **2013**, *38* (12), 4901–4934.

(57) Weng, L. C.; Bell, A. T.; Weber, A. Z. Modeling Gas-Diffusion Electrodes for CO₂ Reduction. *Phys. Chem. Chem. Phys.* **2018**, *20* (25), 16973–16984.

(58) Weber, A. Z.; Borup, R. L.; Darling, R. M.; Das, P. K.; Dursch, T. J.; Gu, W. B.; Harvey, D.; Kusoglu, A.; Litster, S.; Mench, M. M.; et al. A Critical Review of Modeling Transport Phenomena in Polymer-Electrolyte Fuel Cells. *J. Electrochem. Soc.* **2014**, *161* (12), F1254–F1299.

(59) Varcoe, J. R.; Atanassov, P.; Dekel, D. R.; Herring, A. M.; Hickner, M. A.; Kohl, P. A.; Kucernak, A. R.; Mustain, W. E.; Nijmeijer, K.; Scott, K.; et al. Anion-Exchange Membranes in Electrochemical Energy Systems. *Energy Environ. Sci.* **2014**, *7* (10), 3135–3191.

(60) Kusoglu, A.; Weber, A. Z. New Insights into Perfluorinated Sulfonic-Acid Ionomers. *Chem. Rev.* **2017**, *117* (3), 987–1104.

(61) Dekel, D. R. Review of Cell Performance in Anion Exchange Membrane Fuel Cells. *J. Power Sources* **2018**, *375*, 158–169.

(62) Hori, Y.; Murata, A.; Takahashi, R.; Suzuki, S. Electroreduction of Carbon Monoxide to Methane and Ethylene at a Copper Electrode in Aqueous Solutions at Ambient Temperature and Pressure. *J. Am. Chem. Soc.* **1987**, *109* (16), 5022–5023.

(63) Paidar, M.; Fateev, V.; Bouzek, K. Membrane Electrolysis—History, Current Status and Perspective. *Electrochim. Acta* **2016**, *209*, 737–756.

(64) Weber, A. Z.; Kusoglu, A. Unexplained Transport Resistances for Low-Loaded Fuel-Cell Catalyst Layers. *J. Mater. Chem. A* **2014**, *2* (41), 17207–17211.

(65) Tamura, J.; Ono, A.; Sugano, Y.; Huang, C.; Nishizawa, H.; Mikoshiba, S. Electrochemical Reduction of CO₂ to Ethylene Glycol on Imidazolium Ion-Terminated Self-Assembly Monolayer-Modified Au Electrodes in an Aqueous Solution. *Phys. Chem. Chem. Phys.* **2015**, *17* (39), 26072–26078.

(66) Divekar, A. G.; Park, A. M.; Owczarczyk, Z. R.; Seifert, S.; Pivovar, B. S.; Herring, A. M. A Study of Carbonate Formation Kinetics and Morphological Effects Observed on Oh- Form of Pfaem When Exposed to Air Containing CO₂. *ECS Trans.* **2017**, *80* (8), 1005–1011.

(67) Inaba, M.; Jensen, A. W.; Sievers, G. W.; Escudero-Escribano, M.; Zana, A.; Arenz, M. Benchmarking High Surface Area Electrocatalysts in a Gas Diffusion Electrode: Measurement of Oxygen Reduction Activities under Realistic Conditions. *Energy Environ. Sci.* **2018**, *11*, 988.

(68) Wiltshire, R. J. K.; King, C. R.; Rose, A.; Wells, P. P.; Hogarth, M. P.; Thompsett, D.; Russell, A. E. A Pem Fuel Cell for in Situ Xas Studies. *Electrochim. Acta* **2005**, *50* (25), 5208–5217.

(69) Ramaker, D. E.; Korovina, A.; Croze, V.; Melke, J.; Roth, C. Following Orr Intermediates Adsorbed on a Pt Cathode Catalyst During Break-in of a Pem Fuel Cell by in Operando X-Ray Absorption Spectroscopy. *Phys. Chem. Chem. Phys.* **2014**, *16* (27), 13645–13653.

(70) Ishiguro, N.; Saida, T.; Uruga, T.; Nagamatsu, S.-i.; Sekizawa, O.; Nitta, K.; Yamamoto, T.; Ohkoshi, S.-i.; Iwasawa, Y.; Yokoyama, T.; et al. Operando Time-Resolved X-Ray Absorption Fine Structure Study for Surface Events on a Pt₃Co/C Cathode Catalyst in a Polymer Electrolyte Fuel Cell During Voltage-Operating Processes. *ACS Catal.* **2012**, *2* (7), 1319–1330.

(71) Casalongue, H. S.; Kaya, S.; Viswanathan, V.; Miller, D. J.; Friebel, D.; Hansen, H. A.; Nørskov, J. K.; Nilsson, A.; Ogasawara, H. Direct Observation of the Oxygenated Species During Oxygen Reduction on a Platinum Fuel Cell Cathode. *Nat. Commun.* **2013**, *4*, 2817.

(72) Sanchez Casalongue, H. G.; Ng, M. L.; Kaya, S.; Friebel, D.; Ogasawara, H.; Nilsson, A. In Situ Observation of Surface Species on Iridium Oxide Nanoparticles During the Oxygen Evolution Reaction. *Angew. Chem., Int. Ed.* **2014**, *53* (28), 7169–7172.

(73) Zenyuk, I. V.; Parkinson, D. Y.; Hwang, G.; Weber, A. Z. Probing Water Distribution in Compressed Fuel-Cell Gas-Diffusion Layers Using X-Ray Computed Tomography. *Electrochem. Commun.* **2015**, *53*, 24–28.

(74) Medici, E. F.; Zenyuk, I. V.; Parkinson, D. Y.; Weber, A. Z.; Allen, J. S. Understanding Water Transport in Polymer Electrolyte Fuel Cells Using Coupled Continuum and Pore-Network Models. *Fuel Cells* **2016**, *16* (6), 725–733.

(75) Cetinbas, F. C.; Wang, X. H.; Ahluwalia, R. K.; Kariuki, N. N.; Winarski, R. P.; Yang, Z. W.; Sharman, J.; Myers, D. J. Microstructural Analysis and Transport Resistances of Low-Platinum-Loaded Pefc Electrodes. *J. Electrochem. Soc.* **2017**, *164* (14), F1596–F1607.

(76) Komini Babu, S.; Chung, H. T.; Zelenay, P.; Litster, S. Resolving Electrode Morphology's Impact on Platinum Group Metal-Free Cathode Performance Using Nano-Ct of 3d Hierarchical Pore and Ionomer Distribution. *ACS Appl. Mater. Interfaces* **2016**, *8* (48), 32764–32777.

(77) Cetinbas, F. C.; Ahluwalia, R. K.; Kariuki, N.; De Andrade, V.; Fongalland, D.; Smith, L.; Sharman, J.; Ferreira, P.; Rasouli, S.; Myers, D. J. Hybrid Approach Combining Multiple Characterization Techniques and Simulations for Microstructural Analysis of Proton Exchange Membrane Fuel Cell Electrodes. *J. Power Sources* **2017**, *344*, 62–73.

(78) Vermaas, D. A.; Smith, W. A. Synergistic Electrochemical CO₂ Reduction and Water Oxidation with a Bipolar Membrane. *ACS Energy Lett.* **2016**, *1* (6), 1143–1148.

(79) Li, Y. C.; Zhou, D.; Yan, Z.; Gonçalves, R. H.; Salvatore, D. A.; Berlinguette, C. P.; Mallouk, T. E. Electrolysis of CO₂ to Syngas in Bipolar Membrane-Based Electrochemical Cells. *ACS Energy Lett.* **2016**, *1* (6), 1149–1153.